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FORM PTO-1390 (REV. 12-2001)		U.S. DEPARTMENT OF COMMERCE PATENT AND TRADEMARK OFFICE		ATTORNEY'S DOCKET NUMBER	
TRANSMITTAL LETTER TO THE UNITED STATES DESIGNATED/ELECTED OFFICE (DO/EO/US) CONCERNING A FILING UNDER 35 U.S.C. 371				FUK-90	
				U.S. APPLICATION NO. (If known, see 37 CFR 1.5)	
				10/070579	
INTERNATIONAL APPLICATION NO.		INTERNATIONAL FILING DATE		PRIORITY DATE CLAIMED	
PCT/JP00/06191		September 11, 2000		September 9, 1999	
TITLE OF INVENTION APPARATUS FOR HIGH EFFICIENCY GAS TEMPERATURE AND HUMIDITY ADJUSTMENT AND ADJUSTMENT METHOD OF THE SAME					
APPLICANT(S) FOR DO/EO/US					
Tadahiro OHMI et al.					
Applicant herewith submits to the United States Designated/Elected Office (DO/EO/US) the following items and other information:					
<p>1. <input checked="" type="checkbox"/> This is a FIRST submission of items concerning a filing under 35 U.S.C. 371</p> <p>2. <input type="checkbox"/> This is a SECOND or SUBSEQUENT submission of items concerning a filing under 35 U.S.C. 371.</p> <p>3. <input type="checkbox"/> This is an express request to begin national examination procedures (35 U.S.C. 371(f)). The submission must include items (5), (6), (9) and (21) indicated below.</p> <p>4. <input checked="" type="checkbox"/> The US has been elected by the expiration of 19 months from the priority date (Article 31).</p> <p>5. <input checked="" type="checkbox"/> A copy of the International Application as filed (35 U.S.C. 371(c)(2))</p> <p>a. <input type="checkbox"/> is attached hereto (required only if not communicated by the International Bureau).</p> <p>b. <input checked="" type="checkbox"/> has been communicated by the International Bureau.</p> <p>c. <input type="checkbox"/> is not required, as the application was filed in the United States Receiving Office (RO/US).</p> <p>6. <input checked="" type="checkbox"/> An English language translation of the International Application as filed (35 U.S.C. 371(c)(2)).</p> <p>a. <input checked="" type="checkbox"/> is attached hereto.</p> <p>b. <input type="checkbox"/> has been previously submitted under 35 U.S.C. 154(d)(4).</p> <p>7. <input checked="" type="checkbox"/> Amendments to the claims of the International Application under PCT Article 19 (35 U.S.C. 371(c)(3))</p> <p>a. <input type="checkbox"/> are attached hereto (required only if not communicated by the International Bureau)</p> <p>b. <input type="checkbox"/> have been communicated by the International Bureau.</p> <p>c. <input type="checkbox"/> have not been made, however, the time limit for making such amendments has NOT expired</p> <p>d. <input checked="" type="checkbox"/> have not been made and will not be made.</p> <p>8. <input type="checkbox"/> An English language translation of the amendments to the claims under PCT Article 19 (35 U.S.C. 371 (c)(3))</p> <p>9. <input checked="" type="checkbox"/> An oath or declaration of the inventor(s) (35 U.S.C. 371(c)(4)).</p> <p>10. <input type="checkbox"/> An English language translation of the annexes of the International Preliminary Examination Report under PCT Article 36 (35 U.S.C. 371(c)(5)).</p> <p>Items 11 to 20 below concern document(s) or information included:</p> <p>11. <input checked="" type="checkbox"/> An Information Disclosure Statement under 37 CFR 1.97 and 1.98</p> <p>12. <input type="checkbox"/> An assignment document for recording. A separate cover sheet in compliance with 37 CFR 3.28 and 3.31 is included.</p> <p>13. <input checked="" type="checkbox"/> A FIRST preliminary amendment.</p> <p>14. <input type="checkbox"/> A SECOND or SUBSEQUENT preliminary amendment.</p> <p>15. <input type="checkbox"/> A substitute specification.</p> <p>16. <input type="checkbox"/> A change of power of attorney and/or address letter.</p> <p>17. <input type="checkbox"/> A computer-readable form of the sequence listing in accordance with PCT Rule 13ter.2 and 35 U.S.C. 1.821 - 1.825.</p> <p>18. <input type="checkbox"/> A second copy of the published international application under 35 U.S.C. 154(d)(4).</p> <p>19. <input type="checkbox"/> A second copy of the English language translation of the international application under 35 U.S.C. 154(d)(4).</p> <p>20. <input type="checkbox"/> Other items or information:</p>					

U.S. APPLICATION NO. (if known, see 37 CFR 1.53) 10/070579		INTERNATIONAL APPLICATION NO. 		ATTORNEY'S DOCKET NUMBER FUK-90	
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21. <input checked="" type="checkbox"/> The following fees are submitted. BASIC NATIONAL FEE (37 CFR 1.492 (a) (1) - (5)): Neither international preliminary examination fee (37 CFR 1.482) nor international search fee (37 CFR 1.445(a)(2)) paid to USPTO and International Search Report not prepared by the EPO or JPO \$1040.00 International preliminary examination fee (37 CFR 1.482) not paid to USPTO but International Search Report prepared by the EPO or JPO \$890.00 International preliminary examination fee (37 CFR 1.482) not paid to USPTO but international search fee (37 CFR 1.445(a)(2)) paid to USPTO \$740.00 International preliminary examination fee (37 CFR 1.482) paid to USPTO but all claims did not satisfy provisions of PCT Article 33(1)-(4) \$710.00 International preliminary examination fee (37 CFR 1.482) paid to USPTO and all claims satisfied provisions of PCT Article 33(1)-(4) \$100.00 ENTER APPROPRIATE BASIC FEE AMOUNT =				CALCULATIONS PTO USE ONLY	
				\$ 890.00	
Surcharge of \$130.00 for furnishing the oath or declaration later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(e)).				\$ 0	
CLAIMS	NUMBER FILED	NUMBER EXTRA	RATE	\$	
Total claims	16 - 20 =	0	x \$18.00	\$ 0	
Independent claims	3 - 3 =	0	x \$84.00	\$ 0	
MULTIPLE DEPENDENT CLAIM(S) (if applicable)				+ \$280.00	
TOTAL OF ABOVE CALCULATIONS =				\$ 890.00	
<input type="checkbox"/> Applicant claims small entity status. See 37 CFR 1.27. The fees indicated above are reduced by 1/2.				+ \$ 0	
SUBTOTAL =				\$ 890.00	
Processing fee of \$130.00 for furnishing the English translation later than <input type="checkbox"/> 20 <input type="checkbox"/> 30 months from the earliest claimed priority date (37 CFR 1.492(f)).				\$ 0	
TOTAL NATIONAL FEE =				\$ 890.00	
Fee for recording the enclosed assignment (37 CFR 1.21(h)). The assignment must be accompanied by an appropriate cover sheet (37 CFR 3.28, 3 31). \$40.00 per property +				\$ 0	
TOTAL FEES ENCLOSED =				\$ 890.00	
				Amount to be refunded:	\$
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a. ☒ A check in the amount of \$ 890.00 to cover the above fees is enclosed. Check # 5964


b. ☐ Please charge my Deposit Account No. _____ in the amount of \$ _____ to cover the above fees
 A duplicate copy of this sheet is enclosed.

c. ☒ The Commissioner is hereby authorized to charge any additional fees which may be required, or credit any
 overpayment to Deposit Account No 501157. A duplicate copy of this sheet is enclosed.

d. ☐ Fees are to be charged to a credit card **WARNING:** Information on this form may become public. **Credit card
 information should not be included on this form.** Provide credit card information and authorization on PTO-2038.

NOTE: Where an appropriate time limit under 37 CFR 1.494 or 1.495 has not been met, a petition to revive (37 CFR
 1.137 (a) or (b)) must be filed and granted to restore the application to pending status.

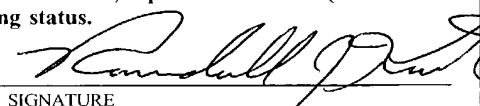
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022855

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SIGNATURE



Randall J. Knuth

NAME

34,644

REGISTRATION NUMBER

IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re of Applicant)
Tadahiro OHMI et al.) Art Group:
Serial No.:)
Filing Date: March 8, 2002)
Title: APPARATUS FOR HIGH) Examiner:
EFFICIENCY GAS TEMPERATURE)
AND HUMIDITY ADJUSTMENT)
AND ADJUSTMENT METHOD OF)
THE SAME)

PRELIMINARY AMENDMENT

Hon. Commissioner of Patents and Trademarks
BOX PCT
Washington, D.C. 20231

Sir:


Applicant hereby submits the following Preliminary Amendment.

REMARKS

The undersigned respectfully submits that with this Preliminary Amendment no new matter has been added.

If the Examiner has any questions or comments that would speed prosecution of this case, the Examiner is invited to call the undersigned at 260/485-6001.

Respectfully submitted,


Randall J. Knuth
Registration No. 34,644

RJK/td

CERTIFICATE OF MAILING

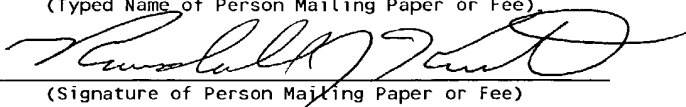
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CLEAN CLAIMS AFTER PRELIMINARY AMENDMENT

1. An apparatus for high efficiency gas temperature and humidity adjustment, comprising a cooling coil; and a condensate water removal means for removing condensate water deposited on said cooling coil.

2. An apparatus for high efficiency gas temperature and humidity adjustment, comprising a cooling coil; and

a means for supplying the cooling coil with deaeration water or hydrogen water as cooling water.

3. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1, wherein said condensate water removal means is a means for spraying compressed gas to the cooling coil.

4. The apparatus for high efficiency gas temperature and humidity adjustment of claim 3, wherein the pressure of said compressed gas is 2 to 10 kgf/cm².

5. The apparatus for high efficiency gas temperature and humidity adjustment of claim 3, wherein said compressed gas is a cooling gas.

6. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1, wherein said condensate water removal means comes physically into contact with the condensate water, and has a function to remove said condensate water.

7. The apparatus for high efficiency gas temperature and

humidity adjustment of claim 6, wherein said condensate water removal means is a brush.

8. The apparatus for high efficiency gas temperature and humidity adjustment of claim 7, wherein said brush is composed to be capable of removing said condensate water by rotation or other displacement.

9. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 wherein cooling fins of said cooling coil are divided every one line or two lines, or have slits for displacement guide disposed every one line or two lines
5 of heat exchange fins.

10. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 wherein the surface of said cooling coil is composed of water-repellent surface.

11. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 comprising a means capable of spraying condensed liquid again.

12. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 wherein a surface treatment using alumite treatment film or the like is applied to the surface of said cooling coil so that the heat transfer efficiency from the
5 surface thereof to the gas by heat radiation be improved.

13. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 wherein an ultrasonic applying

apparatus for applying vibration by ultrasonic waves is comprised on the surface of said cooling coil.

14. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 comprising a means for supplying the cooling water tube of said cooling coil with deaeration water.

15. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 comprising a means for supplying the cooling water tube of said cooling coil with hydrogen water.

16. A method for high efficiency gas temperature and humidity adjustment, the method comprising the steps of, letting flow cooling water in a cooling water tube of a cooling coil, and cooling a gas to be cooled by letting flow the gas to be cooled
5 between cooling fins, wherein deaerated water is used as coil cooling water.

ABSTRACT OF THE DISCLOSURE

An apparatus for high efficiency gas temperature and humidity adjustment and an adjustment method allowing to raise the heat exchange efficiency of a cooling coil, reduce the cooling water quantity, also lower the pipe arrangement diameter and water supply pump power, thereby making it possible to cut
5 the initial cost and running cost of the air-conditioning system.

The apparatus for high efficiency gas temperature and humidity adjustment is characterized by a system for removing condensate water deposited on the cooling coil.

MARKED-UP CLAIMS

1. An apparatus for high efficiency gas temperature and humidity adjustment, comprising a cooling coil; and
a condensate water removal means for removing condensate water deposited on [a] said cooling coil.
2. An apparatus for high efficiency gas temperature and humidity adjustment, comprising a cooling coil; and
a means for supplying the cooling coil with deaeration water or hydrogen water as cooling water.
3. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1, wherein said condensate water removal means is a means for spraying compressed gas to the cooling coil.
4. The apparatus for high efficiency gas temperature and humidity adjustment of claim 3, wherein the pressure of said compressed gas is 2 to 10 kgf/cm².
5. The apparatus for high efficiency gas temperature and humidity adjustment of claim 3 [or 4], wherein said compressed gas is a cooling gas.
6. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1, wherein said condensate water removal means comes physically into contact with the condensate water, and has a function to remove said condensate water.
7. The apparatus for high efficiency gas temperature and

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humidity adjustment of claim 6, wherein said condensate water removal means is a brush.

8. The apparatus for high efficiency gas temperature and humidity adjustment of claim 7, wherein said brush is composed to be capable of removing said condensate water by rotation or other displacement.

5

10. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 [any one of claims 1, 2 to 9,] wherein the surface of said cooling coil is composed of water-repellent surface.

11. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 [any one of claims 1 to 10,] comprising a means capable of spraying condensed liquid again.

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MARKED-UP CLAIMS

heat radiation be improved.

13. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 [any one of claims 1 to 12,] wherein an ultrasonic applying apparatus for applying vibration
5 by ultrasonic waves is comprised on the surface of said cooling coil.

14. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 [any one of claims 1, 3 to 13,] comprising a means for supplying the cooling water tube of said cooling coil with deaeration water.

15. The apparatus for high efficiency gas temperature and humidity adjustment of claim 1 [any one of claims 1, 3 to 13,] comprising a means for supplying the cooling water tube of said cooling coil with hydrogen water.

16. A method for high efficiency gas temperature and humidity [adjustment;] adjustment, the method comprising the steps of, letting flow cooling water in a cooling water tube of a cooling coil, and cooling a gas to be cooled by letting flow the
5 gas to be cooled between cooling fins, wherein [deaeration] deaerated water is used as coil cooling water.

MARKED-UP ABSTRACT

[The present invention has an object to comprise an] An
apparatus for high efficiency gas temperature and humidity
adjustment and an adjustment method allowing to [elevate] raise
the heat exchange efficiency of a cooling coil, reduce the
cooling water quantity, [lower also] also lower the pipe
arrangement diameter and water supply pump power, thereby making
it possible to cut the initial cost and running cost of the air-
conditioning system.

The apparatus for high efficiency gas temperature and humidity adjustment is characterized by [that means] a system for removing condensate water deposited on the cooling coil.

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SPECIFICATION

APPARATUS FOR HIGH EFFICIENCY GAS TEMPERATURE AND HUMIDITY ADJUSTMENT AND ADJUSTMENT METHOD OF THE SAME

5

Field of the Invention

The present invention concerns an apparatus for high efficiency gas temperature and humidity adjustment performing air-conditioning processes such as humidification, dehumidification, rise of temperature, cooling of a gas which is a processed product and an adjustment method of the same.

Background Art

Energy saving equipment is strongly required for air conditioning installation of the future architectural structures. Especially, concerning the running cost of the clean room, the proportion that the electricity charges occupy attains the order of one third of the whole, and most of them concern the power consumed by the air-conditioning installation and process unit. Hence, it is essential for a low lost production to reduce the air-conditioning installation and process unit electric quantity.

The power consumption contributes largely to the operation of air-conditioning facilities. Therefore, the improvement of efficiency of an air-conditioner directly leads to the energy saving.

The enhancement of efficiency of the cooling coil which is one of components composing an air-conditioner leads to the increase of efficiency of the air-conditioner.

Condensate water deposits during the operation on the cooling coil of an air-conditioner in operation. The condensate water results in lowering the cooling effect of an air-conditioned gas. The decrease of efficiency by the fact that the heat-transfer coefficient of condensate water is lower than the heat-transfer coefficient of copper is prevented from removing condensate water deposited on the cooling coil.

The present invention has an object to provide an apparatus

for high efficiency gas temperature and humidity adjustment and an adjustment method allowing to elevate the heat exchange efficiency of the cooling coil, lower the cooling water quantity, reduce the piping diameter and the conveying pump power and cut initial costs and running costs of an air-conditioning system.

Disclosure of the Invention

The apparatus for high efficiency gas temperature and humidity adjustment of the present invention is characterized by that a means for removing condensate water deposited on the cooling coil is provided.

The high efficiency gas temperature and humidity adjustment method of the present invention is a gas temperature and humidity adjustment method for cooling a gas to be cooled by letting a cooling water flow in a cooling tube of an cooling coil and, at the same time, letting the gas to be cooled flow between cooling fins, wherein a deaeration water is used as the cooling water.

The high efficiency gas temperature and humidity adjustment method of the present invention is a gas temperature and humidity adjustment method for cooling a gas to be cooled by letting a cooling water flow in a cooling tube of an cooling coil and, at the same time, letting the gas to be cooled flow between cooling fins, wherein a hydrogen water is used as the cooling water.

The high efficiency gas temperature and humidity adjustment method of the present invention is a gas temperature and humidity adjustment method for cooling a gas to be cooled by letting a cooling water flow in a cooling tube of an cooling coil and, at the same time, letting the gas to be cooled between cooling fins, wherein the cooling is performed after or during the removal of condensate water from the cooling coil.

It should be appreciated that the compressed gas is preferably a cooling gas. In the case of using such cooling gas, there is an advantage that the quantity of heat other than the quantity of heat that should primarily be submitted to a cooling treatment is unnecessary. As for the temperature of cooling gas, 23 to 15 °C is preferable for the reason that there is a difference between the pre-treatment temperature and the post-

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treatment temperature.

Also, it is preferable the surface of the cooling coil be a water repellent surface. For a surface to be water repellent, for instance, a PFA film may be applied to the surface of the cooling
5 coil. Other than the PFA, for example, water-repellent material application and formation of water repellent film are preferable.

In addition, it is preferable to provide means capable of spreading again the condensed liquid. In the case of such composition, there is an advantage that unnecessary heat exchange
10 is not performed, because the condensed liquid temperature and the heat exchanger temperature are equal. As the means capable of spreading again the condensed liquid, for example, it may be configured to draw condensate water by a small pump from a condensate water pan in the air-conditioner, and to spread again
15 from the heat exchanger upper part.

Furthermore, it is preferable to apply an alumite treatment film to the surface of the cooling coil. The adoption of such composition improves the heat-transfer coefficient by heat radiation from the surface thereof to the gas, improving the
20 cooling efficiency.

Brief Description of the Drawings

Fig. 1 is a schematic diagram showing an apparatus for high efficiency gas temperature and humidity adjustment according to
25 the present invention.

Fig. 2 is a schematic perspective view of a cooling coil body according to the present invention.

Fig. 3 is a schematic view of an apparatus for cooling coil condensate water removal according to the present invention.

Fig. 4 is a schematic view of an apparatus for cooling coil
30 condensate water removal according to the present invention.

Fig. 5 is a schematic view of a part of the apparatus for cooling coil condensate water removal according to the present invention.

Fig. 6 is a schematic view of a part of the apparatus for
35 cooling coil condensate water removal according to the present

- | | | |
|----|-----|---|
| | 101 | Air-conditioner main body |
| | 102 | Gas exhaust port |
| | 103 | Gas intake |
| 10 | 104 | Condensate water removal apparatus |
| | 105 | Ventilator fan |
| | 106 | Cooling coil |
| | 107 | Gas sampling pipe arrangement |
| | 108 | Compressor |
| 15 | 109 | Compressed gas supply pipe arrangement |
| | 201 | Cooling coil main body |
| | 202 | Cooling tube |
| | 203 | Cooling tube |
| | 204 | Cooling water return pipe arrangement |
| | 205 | Cooling water supply pipe arrangement |
| 20 | 206 | Cooling fin |
| | 207 | Enter side flow of gas to be cooled |
| | 208 | Exit side flow of gas to be cooled |
| | 301 | Compressed gas pipe arrangement connection port |
| | 302 | Air-conditioner casing |
| 25 | 303 | Compressed gas header |
| | 304 | Cooling coil |
| | 305 | Supply gas before cooling |
| | 306 | Electric motor for driving |
| | 307 | Compressed gas tube |
| 30 | 308 | Guide for movement of compressed gas header |
| | 309 | Supply gas after cooling |
| | 310 | Header stop position |
| | 311 | Compressed gas supply nozzle |
| | 401 | Air-conditioner casing |
| 35 | 402 | Guide for movement of compressed gas header |
| | 403 | Compressed gas header |

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- 404 Compressed gas pipe arrangement connection port
- 405 Electric motor for driving
- 406 Compressed gas tube
- 407 Cooling coil
- 5 408 Compressed gas supply nozzle
- 501 Aluminum fin
- 502 Compressed gas header
- 503 Compressed gas nozzle
- 504 Cooling coil tube
- 10 505 Compressed gas nozzle angle
- 506 Cooling tube alignment angle
- 601 Rotary brush track
- 602 Rotary brush
- 603 Rotating shaft
- 15 604 Heat exchanger
- 605 One end flat brush
- 606 Both ends flat brush
- 607 Heat exchanger

20 Best Mode for Carrying out the Invention

Now, embodiments of the present invention shall be described based on Fig. 1 to Fig. 6.

In an apparatus for high efficiency gas temperature and humidity adjustment, a cooling coil is used to cool a gas to be
 25 adjusted and to adjust the temperature and humidity. Ordinarily, the coil is supplied with a cooling water of around 7 °C, used for lowering the temperature of a gas to be adjusted in contact therewith taking profit of the heat source.

The heat exchange efficiency that lowers under condition
 30 where a water film deposits on the cooling coil is shown by an example described below. Suppose cooling heat quantity by q , heat transmission coefficient of enthalpy reference K_w , coil surface area S , logarithmic mean temperature difference difference MED , internal and external area ratio R , heat conductivity of pipe
 35 inner surface λ_w , scale coefficient of pipe inner surface r_1 , contact thermal resistance between copper pipe, aluminum fin and

pipe r_2 , proportion constant bw , mass-transfer coefficient on fin surface kf , and fin efficiency ϕw , a relation:

$$q = Kw \cdot S \cdot MED$$

$$1 / Kw = R / \dot{a}w + R(r_1 + r_2)bw + 1 / [kf\{\phi w + (1/R)\}]$$

is formed.

Applying general values to the aforementioned formula, the cooling heat quantity becomes about 642 cal/h.

The cooling heat quantity q' at the time when condensate water deposits on the cooling coil in layer, becomes as follows. The compensated value of internal and external area ratio R be R' , and heat transmission coefficient Kw' in the case of deposit of water layer of d in depth on the coil:

$$1/Kw' = R \dot{a}w / zw + R(r_1 + r_2)bw + R' \cdot bw \cdot d / \delta + 1 / [kf\{\phi w + (1/R)\}]$$

$$= 1 / Kw + d / \delta$$

Suppose the water film depth be 1.0 mm, the cooling heat quantity q' becomes about 430 kcal/h.

According to the forgoing, if 1.0 mm of water film deposits on the cooling coil, the heat exchange rates by the coil results in a decrease of about 33 %.

Fig. 1 shows an apparatus for high efficiency gas temperature and humidity adjustment according to an embodiment of the present invention.

The apparatus is configured to blow off by force condensate water deposited on the cooling coil by compressed gas or a brush (rotational brush or flat brush). 101 is a air-conditioner main body, for taking a gas from a gas intake 103 in the air-conditioner main body 101, and discharging temperature and humidity adjusted gas from a gas exit 102 by a fan 105 for transferring the gas. A cooling coil 106 is installed in a passage of gas through the air-conditioner main body 101. A condensate water removal apparatus 104 is installed upstream the cooling coil 106. In the case of using compressed gas, a part of gas taken in by a fan coil is taken in a compressor 108 by a sampling pipe

arrangement 107 to produce a compressed air. A compressed air supply header 104 is supplied with the produced compressed air by a compressed air supply pipe arrangement 109.

5 The blowing pressure of compressed gas to the cooling coil 106 is preferably 2 to 10 kgf/cm², and more preferably 3 to 5 kgf/cm². If the pressure is less than 2 kgf/cm², sometimes condensate water can not be removed sufficiently. On the contrary, if it is excessively higher than 10 kgf/cm², the performance of gas temperature and humidity may be affected.

10 In the forgoing description, a case of using a cooled gas to be cooled of which temperature and humidity are adjusted by the cooling coil 106 as compressed gas has been explained; however a compressed air may be introduced from outside and in the case, it is preferable to adjust the temperature and humidity outside.

15 Fig. 2 is a schematic view of the cooling coil.

The cooling coil is composed by arranging a plurality of cooling fins 206 and cooling water tubes 202, 203 in the cooling coil main body 201. One end of the cooling water tube communicates with a cooling water intake 205 and the other end communicates with a cooling water exit 204.

20 A gas to be cooled 207 passes through between cooling fins 206 each other in the cooling coil main body 201, a cooled gas to be cooled 208 comes out. Cooling water is supplied from the cooling water intake 205, and discharged from the cooling water outlet 204. The cooling water passes through the cooling water tube 202, 203. In order to enhance the cooling efficiency, the cooling fin 206 is installed in a perpendicular direction in respect to the cooling tube 202, 203.

25 Figs. 3 and 4 show respectively a side view and a front view of the compressed gas supply apparatus. The gas to be cooled enters from the drawing right side 309, and flows in the direction of the drawing left side 305. Compressed gas necessary for removing condensate water deposited on the cooling coil of 304 or 407 by the compressed gas supply apparatus is supplied, and 30 condensate water is removed by force from the coil and fin surface by vertical movement the compressed gas supply nozzle 311 or 408,

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using an electric motor for vertical displacement 306 or 405, along a guide for compressed air header displacement of 308 or 402. In the example, the compressed air header 308, 402 reciprocates up and down continuously, and the stop position is supposed to be
5 cooling coil upstream side front. For instance, a gas of pressure about 5.0 kg/cm² is sprayed perpendicularly to the cooling coil, to drop down removed condensate water into a drain pan. 303 or 403 is a compressed gas header, composed of stainless pipe arrangement or the like and provided with discharge nozzles 311 or 408 of
10 compressed gas equidistantly. 308 and 402 is a nozzle up and down guide displacement guide, and the guide is fixed to the air-conditioner main body 302 or 401. Also, the guide 308 or 402 is installed at the right and left of a cooling coil, and is placed at a position not interfering with the gas flow. The compressed
15 gas is supplied from the compressed gas pipe arrangement nozzle 301 or 404 and delivered to the compressed gas nozzle through a flexible tube 307 or 406.

Fig. 5 shows the detail portion of the compressed gas pipe arrangement nozzle.

20 The compressed gas is sprayed from a compressed gas nozzle 503 that has passed through a compressed gas header 502. The position of each nozzle has an angle from the horizontal plane, so that the dropped condensate water flies downward forcibly. By installing the nozzle inclination angle 505 and the cooling tube
25 504 alignment angle 506 equally, installing the nozzle installation position avoiding the cooling fin 501, or other, the compressed gas comes to pass through between cooling fins through the tube effectively, allowing to remove condensate water with a high efficiency to the side removed nozzle. Concerning the cooling
30 tube, as the alignment angle is normally in a range of 30 degrees to 40 degrees, it is preferable to set the nozzle angle also between 30 degrees and 40 degrees.

Fig. 6 shows a schematic view in the case of using a brush (for example, rotational brush, flat brush) in place of compressed
35 gas nozzle. The rotational brush rotates in a range of 601, and a brush 602 made of resin and fixed to a rotation shaft 603 removes

condensate water deposited on the cooling tube and fin.

Besides, it is preferable that the rotation brushes are provided in plurality, and allowed to move between heat exchangers 604 divided into one line or two lines.

5 In addition, in the case of using a flat brush, it is preferable that the shape of the flat brush is formed into the shape of one end 605 or both ends 606 and composed to permit moving between heat exchangers divided into one line or two lines, or moving inside slits of several stages placed every line or two
10 lines of heat exchangers 607 of a continuous number of lines.

On the other hand, it is effective to use a deaeration water as cooling water to circulate in the cooling water tube of the cooling coil, in order to increase the conversion efficiency. Here, the deaeration water means a city water removed gases (especially oxygen) from the city water. The oxygen concentration in the deaeration water is preferably equal or inferior to 10 ppm, more preferably equal or inferior to 5 ppm and still more preferably equal or inferior to 3 ppm. Nevertheless, as the effect saturates under than 1 ppm, 1 to 10 ppm is a preferable range.

Also, it is preferable to use hydrogen water as cooling water for circulation in the cooling water tube of the cooling coil. Hydrogen water is a hydrogenated water, and it is further preferable to use a water wherein the deaeration water is hydrogenated. The hydrogen concentration in the hydrogen water is preferably 0.5 to 1.5 ppm.

Embodiments

Hereinbelow, results of removal of condensate water deposited on the cooling coil 304 or 407 of an air-conditioner, by the apparatus of the present invention.

(Embodiment 1)

The cooling coil was supplied with a cooling water of 7 °C and the cooling water temperature was measured at the cooling water exit.

As parameter of that time, experiments were performed for a

case where condensate water deposits on the coil, a case of removing condensate water with compressed gas using the apparatus shown in Fig. 1, a case of applying the coil surface treatment, and a case of using deaeration water, hydrogen water as cooling water, and they were compared each other.

Keep cooling water supply conditions and intake gas temperature constant, and measure gas output temperature and cooling water output temperature. The gas output temperatures in the case of operating the condensate water removal apparatus, in the case of not operating, and in the case of not processing were compared.

It should be appreciated that the experiment is performed under the condition of simultaneity, in order to impose the same condition to the intake gas temperature. Fig. 7 shows measurement results of gas output temperature.

In Fig. 7, ● shows results of the example and ■ results of a comparison example.

It was confirmed that the removed heat quantity by coil is more effective in the case of removing condensate water than the case without removal, because the gas exit temperature in the case of removing condensate water (●) is lower than the case without removal (■).

(Embodiment 2)

The comparison was performed between the one where PFA film of water-repellent fluorine base resin is applied to the outer surface of the cooling coil and a case without film.

Removal of condensate water was performed by compressed gas similarly to the Embodiment 1.

It should be appreciated that the thickness of PFA film is preferably about 0.5 to 1.0 mm. Adopting such thickness, the thermal efficiency degradation due to film can be limited to the minimum, and at the same time, condensate water is prevented from depositing, and the removal of deposited condensate water can be facilitated.

By the experiment of the time, the condensate water removal

apparatus was operated. It was confirmed that it is more effective in the case of applying a surface treatment than the case without surface treatment, because the gas exit temperature in the case of applying the surface treatment by film of water-repellent resin (Fig. 7▲) is lower than that in the case without application (Fig. 7 ■) thereof.

(Embodiment 3)

In the example, the comparison was performed between the one where alumite treatment is applied to the outer surface of the cooling coil and a case without film.

Removal of condensate water was performed by compressed gas similarly to the Embodiment 1.

In the experiment of this time, the condensate water removal apparatus was operated. It was confirmed that it is more effective in the case of applying a surface treatment such as alumite treatment than the case without surface treatment, because the gas exit temperature in the case of applying a surface treatment by alumite treatment (Fig. 7 ○) is lower than that in the case without application (Fig. 7 ■).

(Embodiment 4)

The comparison was performed between a case where ultrasonic waves are applied to the cooling coil and a case without application.

In the experiment of this time, the condensate water removal apparatus was operated. An ultrasonic element is fixed to a cooling coil plate portion 206 and, furthermore, connected and fixed to the ultrasonic element and a frame section of the apparatus for gas temperature and humidity adjustment. Condensate water deposited on the cooling coil is removed by oscillating the cooling coil main body through the vibration of the ultrasonic element. The frequency of the ultrasonic waves to be used is set to 20 to 50 kHz. This is because under 20 kHz the sound wave energy is insufficient, and, over 50 kHz, there is every possibility of reducing considerably the life of the ultrasonic

element.

It was confirmed that it is more effective in the case of applying ultrasonic waves than the case without application treatment thereof, because the gas exit temperature in the case of
5 applying vibration to the cooling coil by ultrasonic waves (Fig. 7 □) is lower than that in the case without application (Fig. 7 ■).

(Embodiment 5)

By using deaeration water, scale is prevented from generating
10 in the cooling water tube, and the conversion efficiency is prevented from deprecating by scale generation.

The comparison was performed between a case where city water is used as cooling water to circulate in the cooling coil and a case of using deaeration water.

15 As deaeration water, city water removed oxygen was used. The oxygen concentration after deaeration is 3 ppm.

Test results are shown in Fig. 8. In the experiment of this time, the condensate water removal apparatus was operated. The measurement was performed after letting cooling water flow through
20 the cooling coil for 2000 hours continuously.

It was confirmed that it is more effective in the case of using deaeration water than that in the case of using city water, because the gas exit temperature in the case of letting flow the deaeration water (Fig. 8 ●) is lower than the case of city water
25 (Fig. 8 ■).

It should be appreciated that, in the case also of not removing condensate water, results demonstrating that the exit temperature is lower in the case of using deaeration water than the case of using city water were also obtained.

30 It should be appreciated that particularly good results were obtained not more than 10 ppm when the experiment was carried out by changing the oxygen concentration in a range of 0.5 to 20 ppm.

(Embodiment 6)

35 By using hydrogen water, scale is prevented from generating in the cooling water tube, and the conversion efficiency is

prevented from deprecating by scale generation.

The comparison was performed between a case where city water is used as cooling water to circulate in the cooling coil and a case of using hydrogen water.

5 As hydrogen water, city water removed oxygen and thereafter hydrogenated was used. The hydrogen concentration after hydrogenation is 0.6 ppm.

Test results are shown in Fig. 8.

10 In the experiment of this time, the condensate water removal apparatus was operated. The measurement was performed after letting cooling water flow through the cooling coil for 2000 hours continuously.

15 It was confirmed that it is more effective in the case of letting flow hydrogen water than the case of using city water, because the gas exit temperature in the case of letting flow the hydrogen water (Fig. 8○) is lower than that in the case of city water (Fig. 8■).

It should be appreciated that, a similar trend was also obtained in the case of not removing condensate water.

20 Industrial Applicability

According to the present invention, the heat exchange efficiency of the cooling coil elevates, the cooling water quantity can be reduced, the pipe arrangement diameter and water supply pump power also can be lowered, making possible to cut the
25 initial cost and running cost of the air-conditioning system.

What is Claimed is:

1. An apparatus for high efficiency gas temperature and humidity adjustment, comprising a condensate water removal means
5 for removing condensate water deposited on a cooling coil.
2. An apparatus for high efficiency gas temperature and humidity adjustment, comprising a means for supplying the cooling coil with deaeration water or hydrogen water as cooling water.
3. The apparatus for high efficiency gas temperature and
10 humidity adjustment of claim 1, wherein said condensate water removal means is a means for spraying compressed gas to the cooling coil.
4. The apparatus for high efficiency gas temperature and humidity adjustment of claim 3, wherein the pressure of said
15 compressed gas is 2 to 10 kgf/cm².
5. The apparatus for high efficiency gas temperature and humidity adjustment of claim 3 or 4, wherein said compressed gas is a cooling gas.
6. The apparatus for high efficiency gas temperature and
20 humidity adjustment of claim 1, wherein said condensate water removal means comes physically into contact with the condensate water, and has a function to remove said condensate water.
7. The apparatus for high efficiency gas temperature and humidity adjustment of claim 6, wherein said condensate water
25 removal means is a brush.
8. The apparatus for high efficiency gas temperature and humidity adjustment of claim 7, wherein said brush is composed to be capable of removing said condensate water by rotation or other displacement.
9. The apparatus for high efficiency gas temperature and
30 humidity adjustment of any one of claims 1 to 8, wherein cooling fins of said cooling coil are divided every one line or two lines, or have slits for displacement guide disposed every one line or two lines of heat exchange fins.
10. The apparatus for high efficiency gas temperature and
35 humidity adjustment of any one of claims 1, 2 to 9, wherein the

surface of said cooling coil is composed of water-repellent surface.

11. The apparatus for high efficiency gas temperature and humidity adjustment of any one of claims 1 to 10, comprising a means capable of spraying condensed liquid again.

12. The apparatus for high efficiency gas temperature and humidity adjustment of any one of claims 1 to 9, wherein a surface treatment using alumite treatment film or the like is applied to the surface of said cooling coil so that the heat transfer efficiency from the surface thereof to the gas by heat radiation be improved.

13. The apparatus for high efficiency gas temperature and humidity adjustment of any one of claims 1 to 12, wherein an ultrasonic applying apparatus for applying vibration by ultrasonic waves is comprised on the surface of said cooling coil.

14. The apparatus for high efficiency gas temperature and humidity adjustment of any one of claims 1, 3 to 13, comprising a means for supplying the cooling water tube of said cooling coil with deaeration water.

15. The apparatus for high efficiency gas temperature and humidity adjustment of any one of claims 1, 3 to 13, comprising a means for supplying the cooling water tube of said cooling coil with hydrogen water.

16. A method for high efficiency gas temperature and humidity adjustment; comprising the steps of, letting flow cooling water in a cooling water tube of a cooling coil, and cooling a gas to be cooled by letting flow the gas to be cooled between cooling fins, wherein deaeration water is used as coil cooling water.

ABSTRACT

The present invention has an object to comprise an apparatus for high efficiency gas temperature and humidity adjustment and an adjustment method allowing to elevate the heat exchange efficiency of a cooling coil, reduce the cooling water quantity, lower also the pipe arrangement diameter and water supply pump power, making possible to cut the initial cost and running cost of the air-conditioning system.

10 The apparatus for high efficiency gas temperature and humidity adjustment is characterized by that means for removing condensate water deposited on the cooling coil.

FIG.2

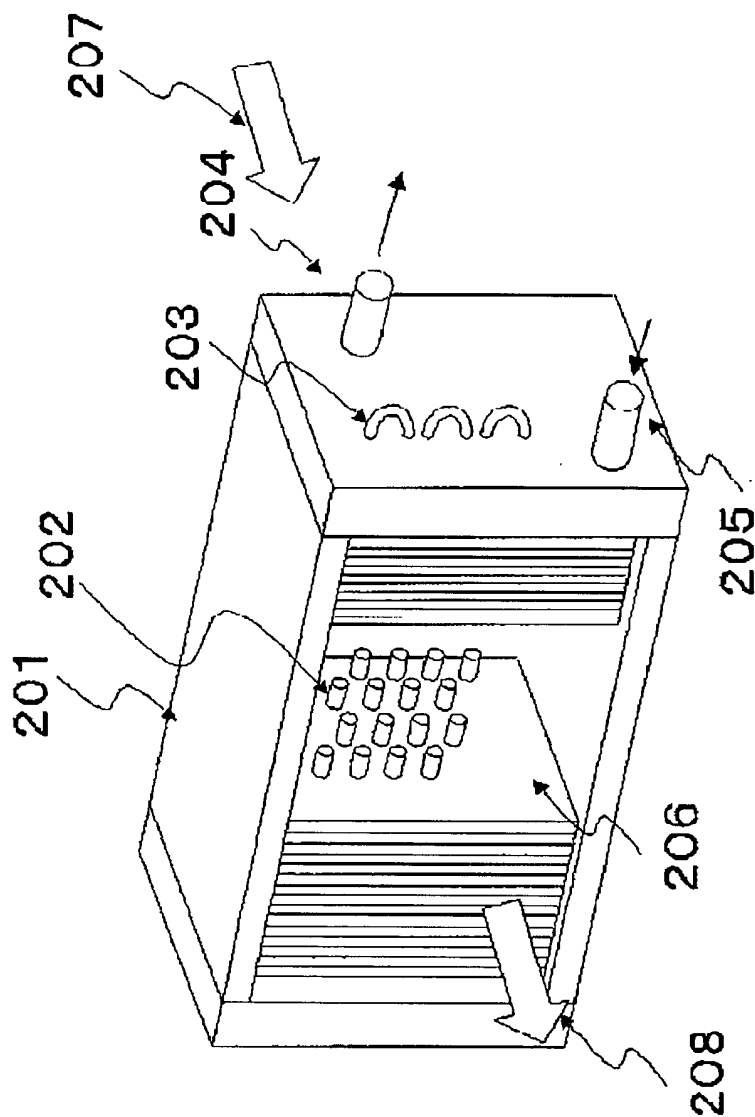


FIG.3

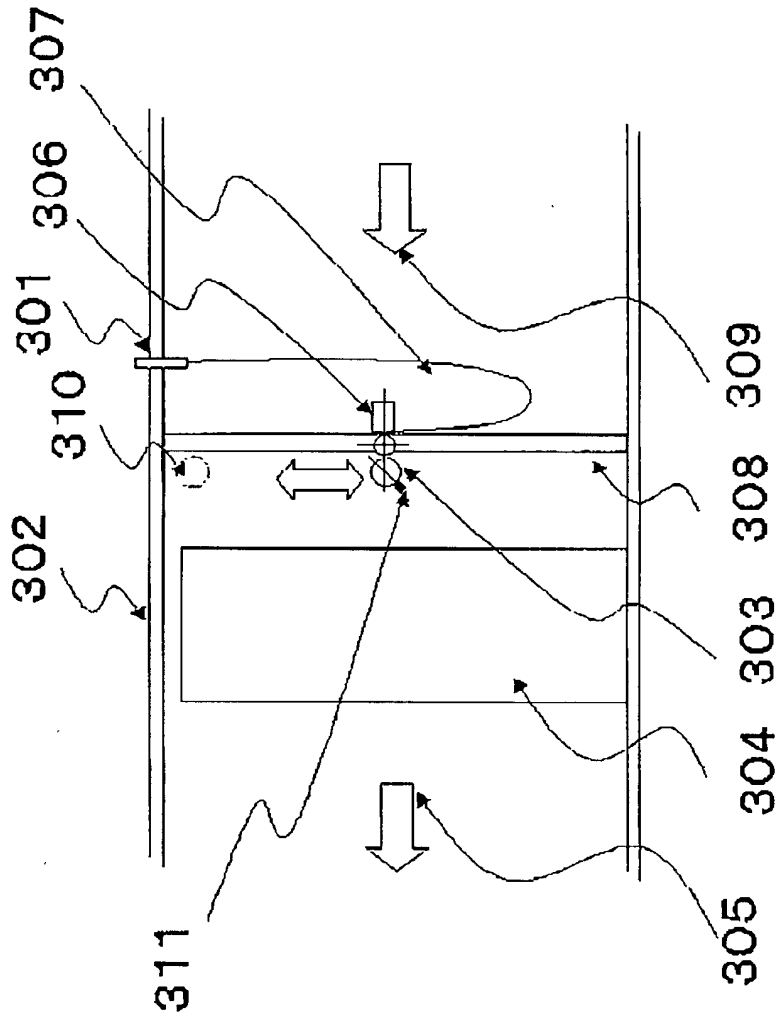


FIG.4

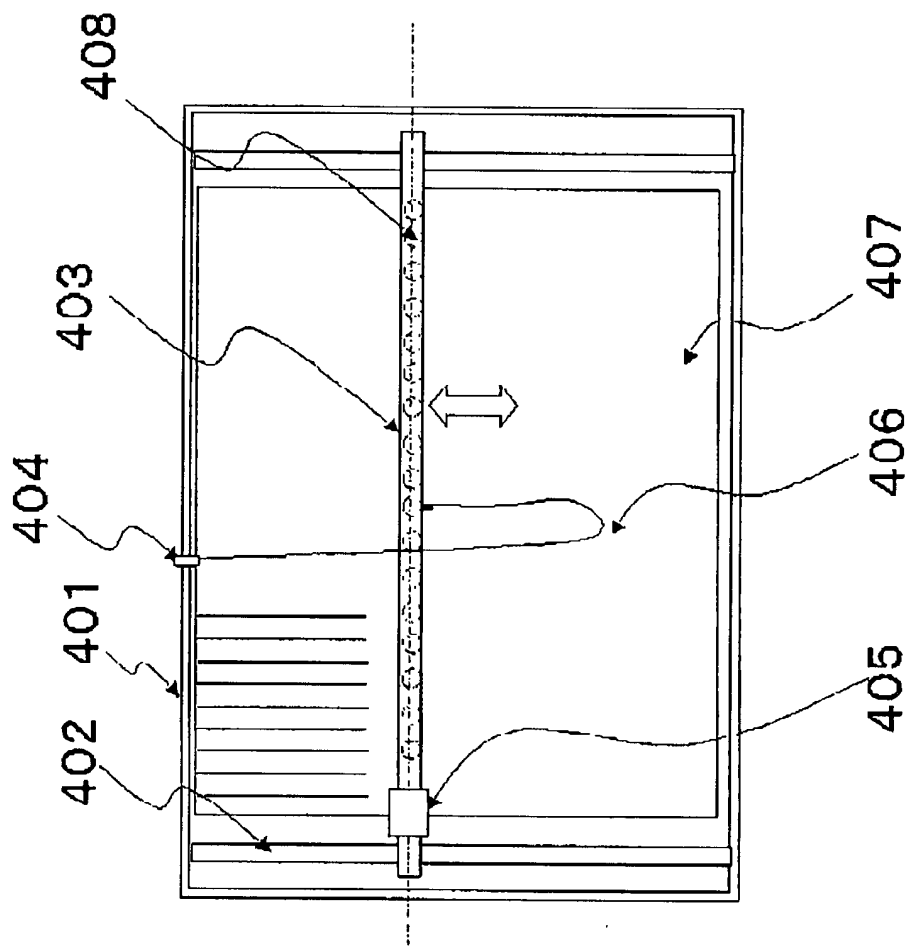


FIG.5

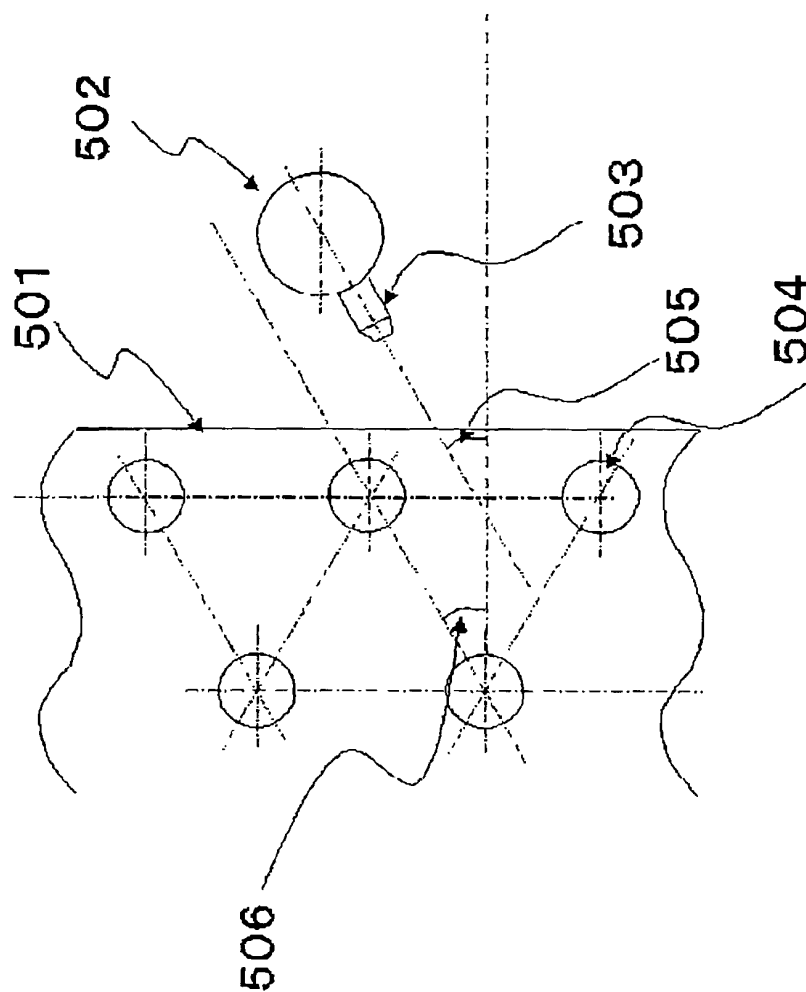


FIG.6

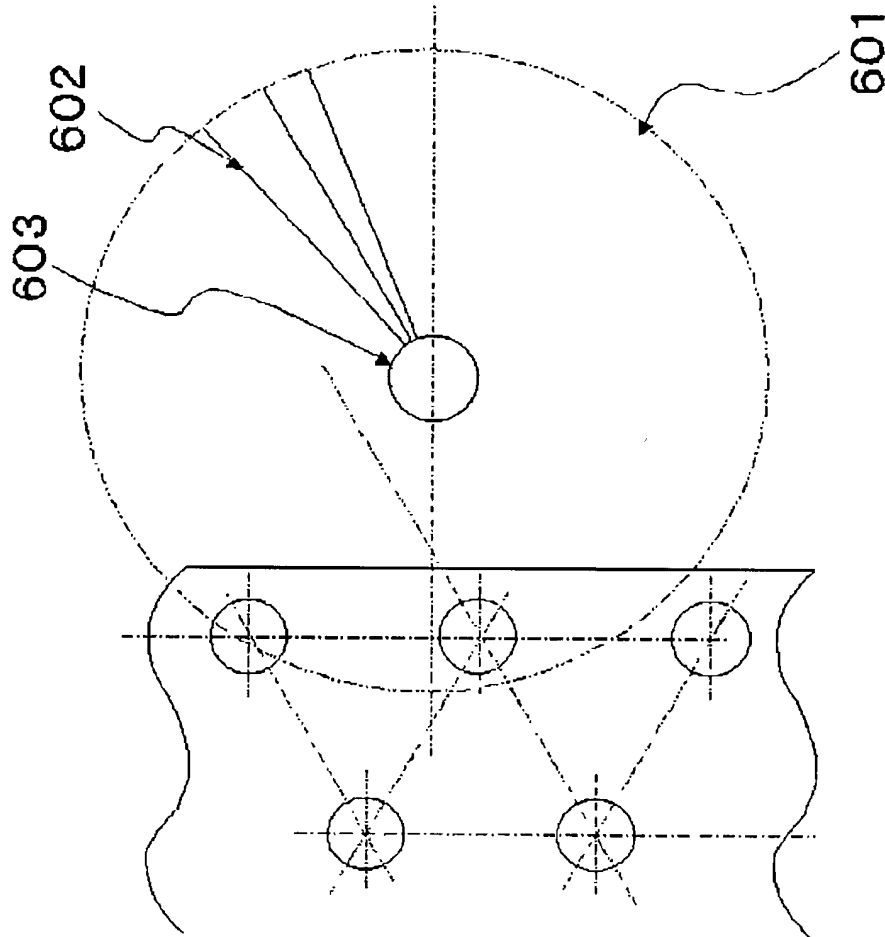


FIG.7

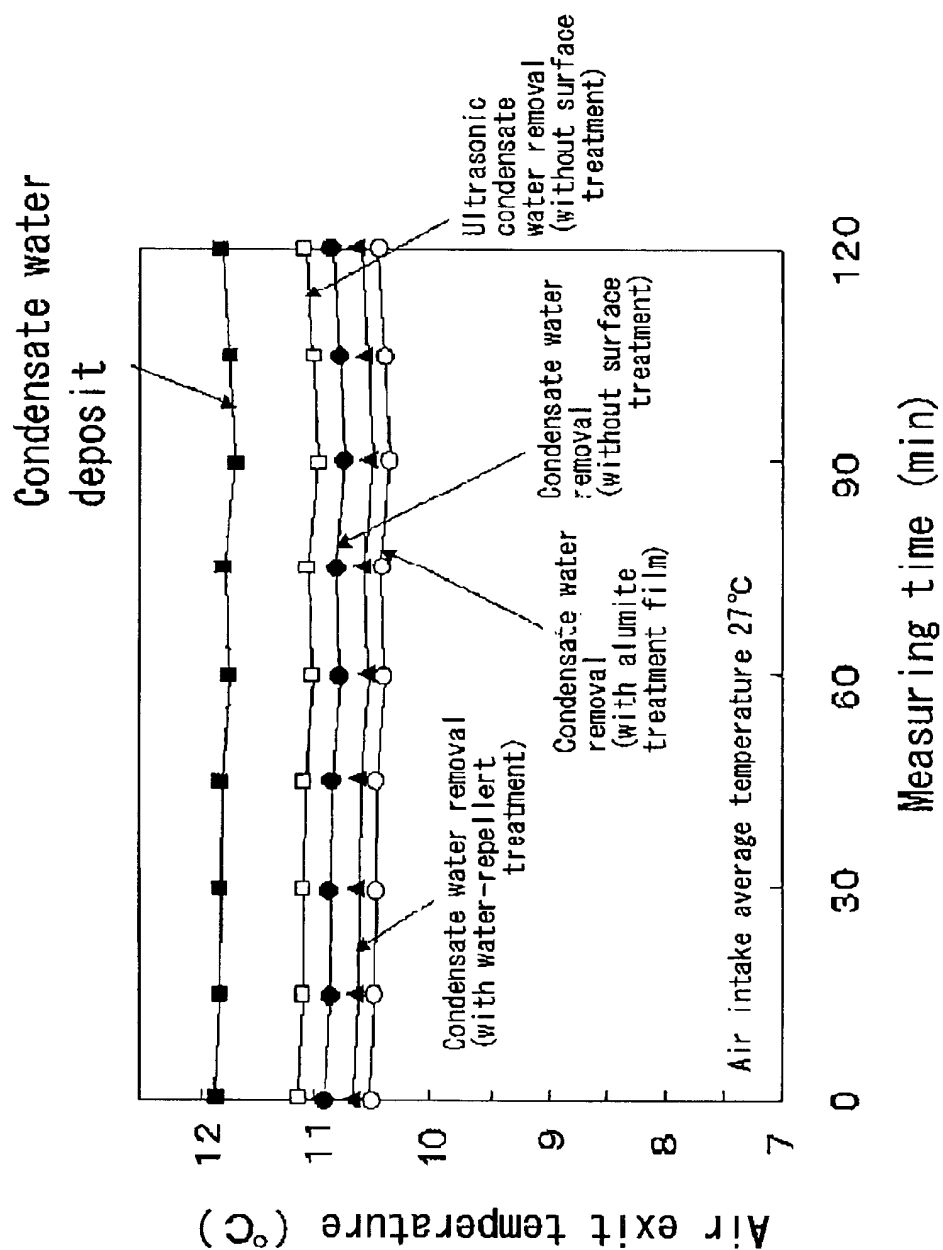
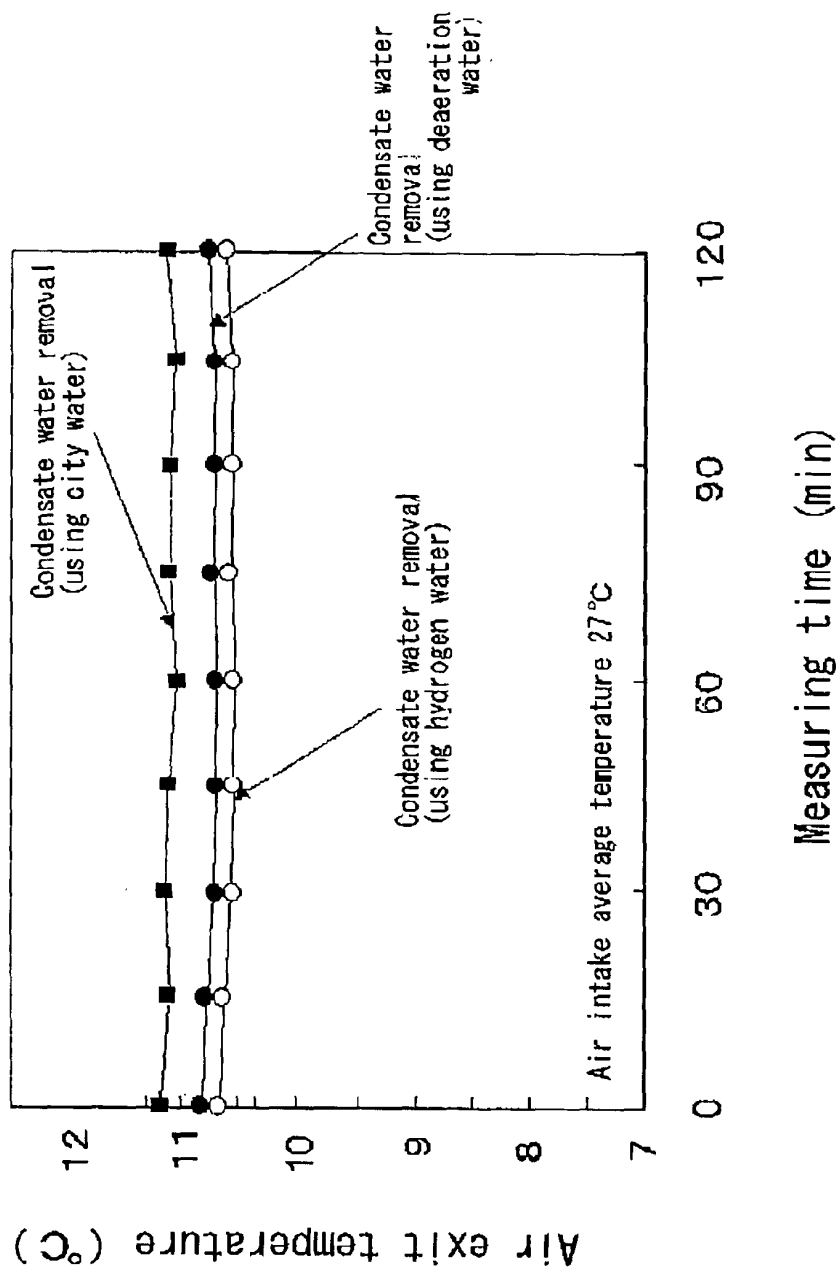


FIG.8



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PCT/USA NATIONAL DECLARATION AND POWER OF ATTORNEY
FOR U.S. PATENT APPLICATIONS
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UNDER 35 U.S.C. SECTION 371(c)(4)

ATTORNEY'S DOCKET NO. FUK-90

As a below named inventor, we hereby declare that:

Our residence, post office address and citizenship are as stated below next to my name:

I verily believe I am the original, first and sole inventor (if only one name is listed below) or a joint inventor (if plural inventors are named below) of the invention described and claimed in international application No. PCT/JP00/06191 entitled: APPARATUS FOR HIGH EFFICIENCY GAS TEMPERATURE AND HUMIDITY ADJUSTMENT AND ADJUSTMENT METHOD OF THE SAME and as amended on _____ (if any), which I have reviewed, and I understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above and for which I solicit a patent; that I do not know and do not believe that this invention was ever known or used in the United States of America before my or our invention or discovery thereof, or patented or described in any printed publication in any country before my or our invention or discovery thereof, or more than one year prior to my international application; that this invention was not in public use or on sale in the United States of America for more than one year prior to my international application; that this invention has not been patented or made the subject of an inventor's certificate issued before the date of my international application in any country foreign to the United States or America on an application filed by me or my legal representatives or assigns more than twelve months before my international application; that I acknowledge my duty to disclose information of which I am aware which is material to the examination of this application; and that prior to filing said international application, applications for patent or inventor's certificate on this invention of discovery which have been filed by me or my legal representatives or assigns in any country foreign to the United States of America are as follows:

(a) none filed more than 12 months prior to said international application, unless named below:

(b) earliest filed less than 12 months prior to said international application (the priority of which is hereby claimed under 35 U.S.C. Section 365):

Japanese Patent Application No. 11-255964 filed September 9, 1999

I hereby claim the benefit under Title 35, United States Code, §120, of any United States application(s) listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States application in the manner provided by the first paragraph of Title 35, United States Code, §112, I acknowledge the duty to disclose material information as defined in Title 37, Code of Federal Regulations, §1.56(a), which occurred between the filing date of the prior application and the national or PCT international filing date of this application.

(Application Serial No.)

(Filing Date)

(Status)(patented, pending, abandoned)

3- I hereby appoint Randall J. Knuth, Regis. No. 34,644, Victor F. Lohmann, III, Regis. No. 33,951 and Vincent P. Merz, Jr., Regis. No. 45,722 of the firm of RANDALL J. KNUTH, P.C., as attorney(s) to prosecute this application and transact all business in the Patent and Trademark Office connected therewith.

I declare further that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

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